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COURSE BROCHURE

Advanced Proportional-Integral-Derivative Loop Tuning for Power Plants Training Course

4 – 15 January 2027
Singapore

Advanced Proportional-Integral-Derivative Loop Tuning for Power Plants Training Course

Ref: 2589_98494 **Date:** 4 – 15 January 2027 **Location:** Singapore **Fees:** 12000 GBP

Advanced Proportional-Integral-Derivative Loop Tuning for Power Plants is a 2-week training course for control and instrumentation engineers who set, test and defend controller settings on boilers, turbines, feedwater systems and auxiliary plant, and who leave with a signed loop tuning record for one generating unit. As units cycle harder to follow variable demand, poorly tuned loops cost efficiency, equipment life and trip margin. Jupiter Prime Training delivers this course for engineers responsible for proportional-integral-derivative loop tuning in generating plant.

Why Proportional-Integral-Derivative Loop Tuning Matters Now

Generating units that once ran at steady base load now ramp, cycle and start several times a week as variable renewable output reshapes dispatch. Each ramp exposes sluggish or oscillating loops in drum level, steam temperature, furnace pressure and deaerator control. Operations teams switch loops to manual when they lose trust, while asset owners see the result in tube stress, valve wear and lost heat rate. A plant that tunes loops from measured dynamics holds tighter limits and ramps with confidence; one that tunes by trial accepts hidden losses and nuisance trips. The course rests on step-test identification, frequency response reasoning and loop performance indices used across process and power industries.

Who Gains Most from Proportional-Integral-Derivative Loop Tuning

- Engineers who own the distributed control logic of a generating unit and approve controller setting changes
- Instrument specialists responsible for transmitter, positioner and final element health on critical loops
- Commissioning engineers who bring new or refurbished boilers, heat recovery units and auxiliaries into automatic control
- Performance engineers who link loop behaviour to heat rate, emissions and ramp capability
- Operations support engineers who investigate loops placed in manual and restore operator confidence

Plant teams that send a control engineer, an instrument specialist and an operations support engineer together gain most, because the tuning record they build needs all three views.

Proportional-Integral-Derivative Loop Tuning Capabilities

Participants move from guessing gains to deriving them from the measured dynamics of each loop and proving the result on recorded trends.

- Identify process gain, dead time and time constants from bump tests — the choice of tuning method for each loop
- Calculate controller gain, integral time and derivative time from identified models — the setting change submitted for approval
- Design cascade, feedforward and ratio schemes — unit ramp capability agreed with operations
- Assess loop performance with variability and oscillation indices — the priority list for maintenance planners
- Diagnose valve stiction, backlash and sensor faults — the decision to tune or repair first
- Build a loop tuning record with before and after evidence — plant management and audit reviewers

Key Proportional-Integral-Derivative Loop Tuning Terms

- Dead time — the delay between a controller output change and the first visible response of the measured variable.
- Integral time — the controller setting that sets how quickly accumulated error moves the output to remove offset.
- Cascade control — an arrangement where an outer controller sets the target of a faster inner controller on the same process.
- Feedforward — control action calculated from a measured disturbance before it upsets the controlled variable.
- Stiction — static friction in a valve that makes it stick and then jump, often causing a steady oscillation.
- Robustness margin — how far process dynamics can change before a tuned loop becomes oscillatory or unstable.

Proportional-Integral-Derivative Loop Tuning Day by Day

Day 1: Loop Behaviour in Cycling Generating Units

- Flexible Operation Demands — Which Loops Limit Unit Ramp Rate
- Loop Inventory by Criticality — Where Tuning Effort Goes First
- Manual Mode Audit — Why Operators Lose Trust in Automatic Control
- Controller Algorithm Forms — Ideal, Series and Parallel Setting Conversion
- Loop Tuning Record Template — Evidence Expected Before Any Change

Day 2: Identifying Process Dynamics

- Open Loop Bump Test Planning — Safe Step Size and Operating Point
- First Order Plus Dead Time Fitting — Model Choice for Tuning
- Integrating Process Identification — Drum Level and Tank Behaviour
- Closed Loop Test Methods — Identification Without Taking Loops Off Line
- Nonlinear Gain Mapping — Settings Across the Load Range

Day 3: Tuning Rules and Their Limits

- Lambda Tuning — Choosing Closed Loop Speed Against Robustness
- Internal Model Control Rules — Settings From Identified Models
- Ultimate Gain Method — When Sustained Cycling Tests Are Acceptable
- Derivative Filtering — Noise Sensitivity Versus Faster Recovery
- Setpoint Weighting — Response to Operator Changes Versus Disturbances

Day 4: Final Elements and Measurement Quality

- Valve Signature Testing — Stiction and Backlash Before Retuning
- Positioner Response Checks — Inner Loop Speed of the Final Element
- Transmitter Damping and Filtering — Hidden Lag Added to Loops
- Variable Speed Drive Actuation — Fan and Pump Control Response
- Repair or Retune Decision Tree — Maintenance Request Versus Setting Change

Day 5: Cascade Control on Boilers

- Cascade Structure Design — Inner Loop Speed Ratio Requirements
- Tuning Order for Cascades — Inner Loop First, Then Outer
- Steam Temperature Attemperation Cascade — Spray Valve and Outlet Control
- Furnace Pressure Control — Induced Draught Fan Response
- Output Tracking and Bumpless Transfer — Safe Mode Switching

Day 6: Feedforward and Ratio Schemes

- Three Element Drum Level Control — Steam Flow Feedforward Design
- Air to Fuel Ratio With Cross Limiting — Combustion Safety During Ramps
- Load Demand Feedforward to Firing Rate — Faster Unit Response
- Dynamic Compensation With Lead and Lag — Matching Disturbance Timing
- Feedforward Gain Scheduling — Adjusting Action With Unit Load

Day 7: Interacting Loops and Coordinated Control

- Relative Gain Analysis — Pairing Inputs With Controlled Variables
- Boiler Turbine Coordinated Control — Pressure and Megawatt Trade-Off
- Decoupling Strategies — Reducing Interaction Between Neighbouring Loops
- Override and Selector Control — Protecting Equipment Limits Automatically
- Integral Windup Protection — Recovery After Saturation or Override

Day 8: Measuring Loop Performance

- Variability and Error Indices — Ranking Loops Across a Unit
- Oscillation Detection From Historian Trends — Finding Root Loops
- Minimum Variance Benchmarking — Room Left for Improvement
- Time in Automatic and Saturation Statistics — Operator Confidence Measures
- Performance Reporting Dashboard — Monthly Review With Maintenance

Day 9: Simulation and Safe Change Control

- Loop Simulation From Identified Models — Testing Settings Off Line
- Robustness Checks Across Load Points — Margin Before Implementation
- Management of Change for Settings — Approval, Rollback and Records
- Protection System Interfaces — Keeping Tuning Clear of Trip Logic
- Operator Briefing on New Responses — Handover to the Control Room

Day 10: Practising the Loop Tuning Record

- Bump Test Data Set Analysis — Applying Model Fitting to a Live Case
- Cascade and Feedforward Redesign — Applying Days Five and Six
- Valve and Sensor Diagnosis on Case Trends — Applying Final Element Checks
- Peer Review of Proposed Settings — Challenge Before Approval
- Completed Loop Tuning Record — Unit Evidence Ready for Sign-Off

Applying Proportional-Integral-Derivative Loop Tuning After the Course

- Run bump tests on the three loops most often in manual, fit dead time models and propose lambda-based settings for approval.
- Rank every loop on one unit with variability and oscillation indices and send valve signature requests for the worst five.

Proportional-Integral-Derivative Loop Tuning Questions FAQ

What is proportional-integral-derivative loop tuning for power plants and why does it matter now?

It is the practice of setting controller gains from measured plant dynamics. It matters now because generating units ramp and cycle far more often, and loops tuned for steady load oscillate, drift or end up in manual, costing efficiency and equipment life.

Which roles gain most from proportional-integral-derivative loop tuning for power plants?

Control engineers who approve setting changes gain most, alongside instrument, commissioning, performance and operations support engineers. You benefit when you own loops on boilers, turbines or auxiliaries and must prove a change improves behaviour.

How does proportional-integral-derivative loop tuning for power plants differ from a general instrumentation course?

It goes deeper into tuning than a broad instrumentation course. A general course covers measurement, valves and control system architecture, while this one spends two weeks on identifying dynamics, deriving settings, designing cascade and feedforward schemes and proving results on generating plant.

What do you bring back from proportional-integral-derivative loop tuning for power plants?

You bring back a completed tuning record for one unit. It holds identified models, proposed settings, valve diagnosis, simulation checks and before and after trends, ready for peer review and approval in your own plant.

Proportional-Integral-Derivative Loop Tuning: The Way Forward

The loop tuning record first informs which loops on a unit receive new settings and which need valve or sensor repair before any retuning. Control engineers, maintenance planners and shift supervisors all draw on it. After its first use, revisit the identified models at a different load point, since dynamics shift as the unit cycles and settings that held at full load may not hold at minimum.